
CAP.C534

Advanced Supercritical Fluid Process

(超臨界流体プロセス特論)

1. Fundamental Property of Supercritical Fluid

Department of Chemical Science and Engineering

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2018.9.27 Room 421 of South Buld. 4

New development of Chemical Process

- Reaction process : rapid, selective, simple
- Separation process : rapid, low energy, selective
- Material process : low cost and energy, functional material

How to use and design “Supercritical fluid medium”
for development of chemical process

Fundamentals

Reaction mechanism

Separation mechanism

Material design

Supercritical Fluid

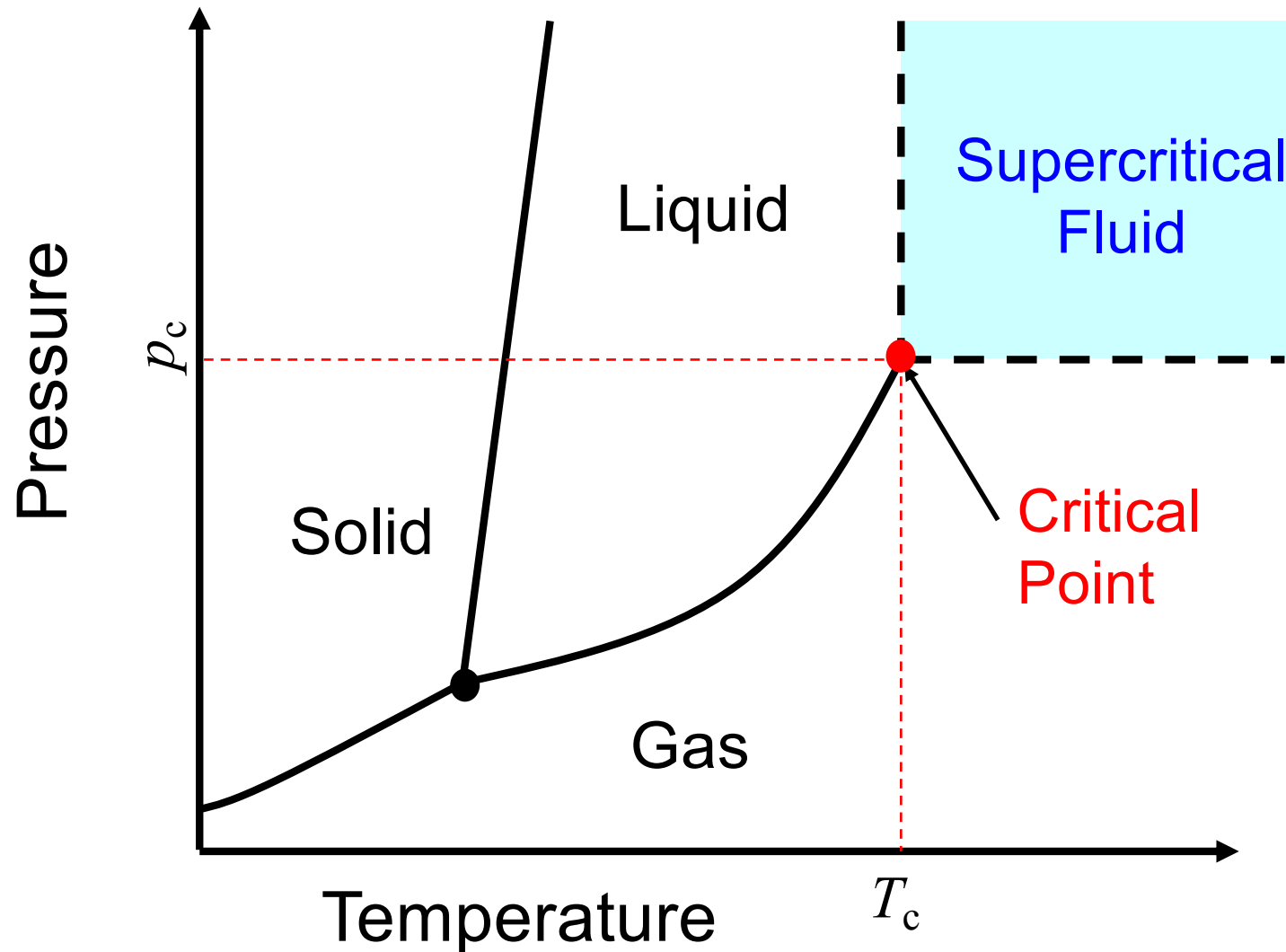
1. 9/27 Fundamental property of SCF
2. 10/4 Particle formation using SCF (I)
3. 10/11 Particle formation using SCF (II)
4. 10/18 Porous material formation using SCF (I)
5. 10/25 Porous material formation using SCF (II)
6. 11/1 Composite formation using SCF
7. 11/8 Film formation using SCF
- 11/22 Final report submission

Class document will be upload in OCW

Supercritical Fluid

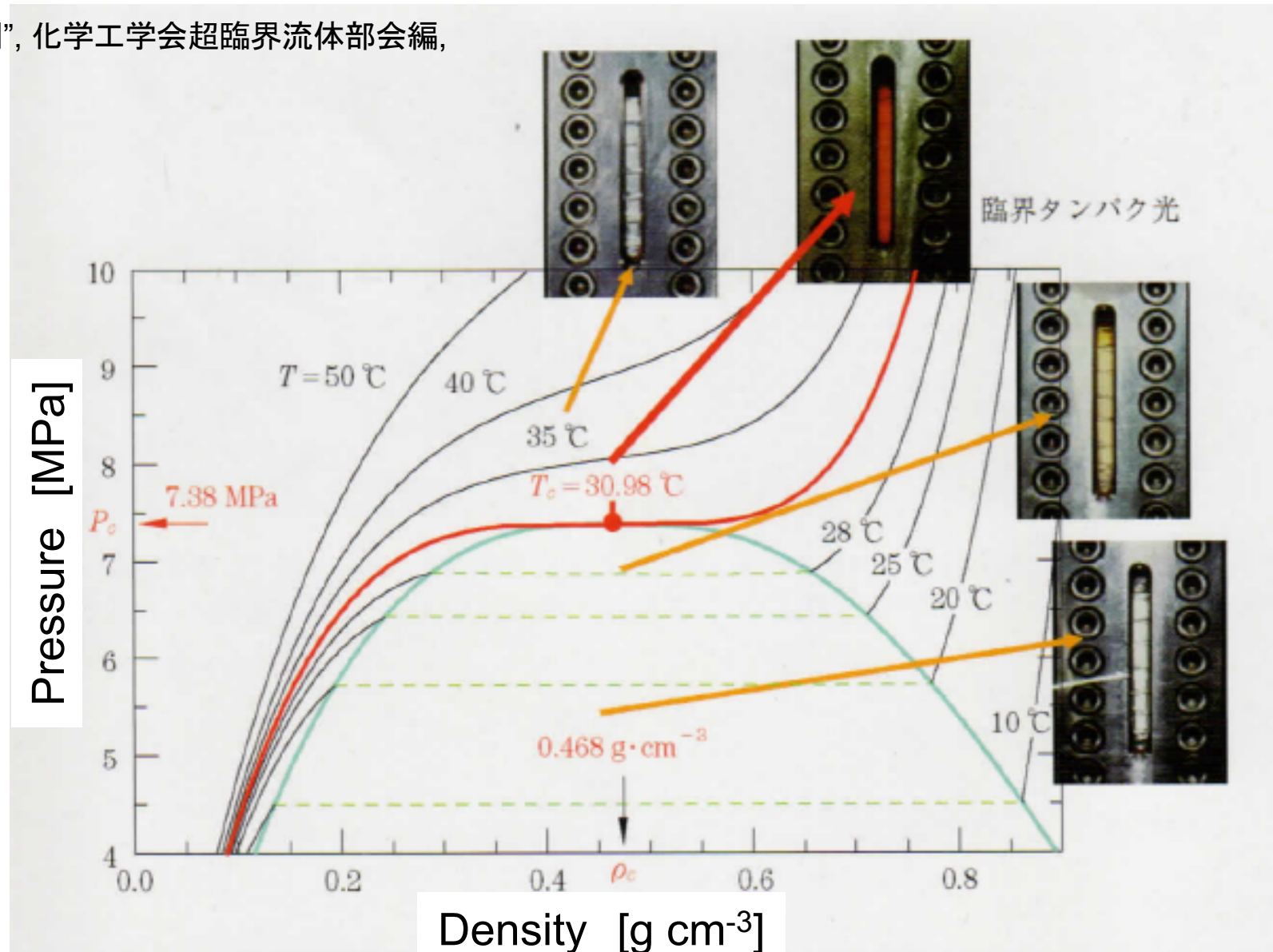
4

➤ Phase diagram of pure compound



➤ Specific phase “color” change of SCF

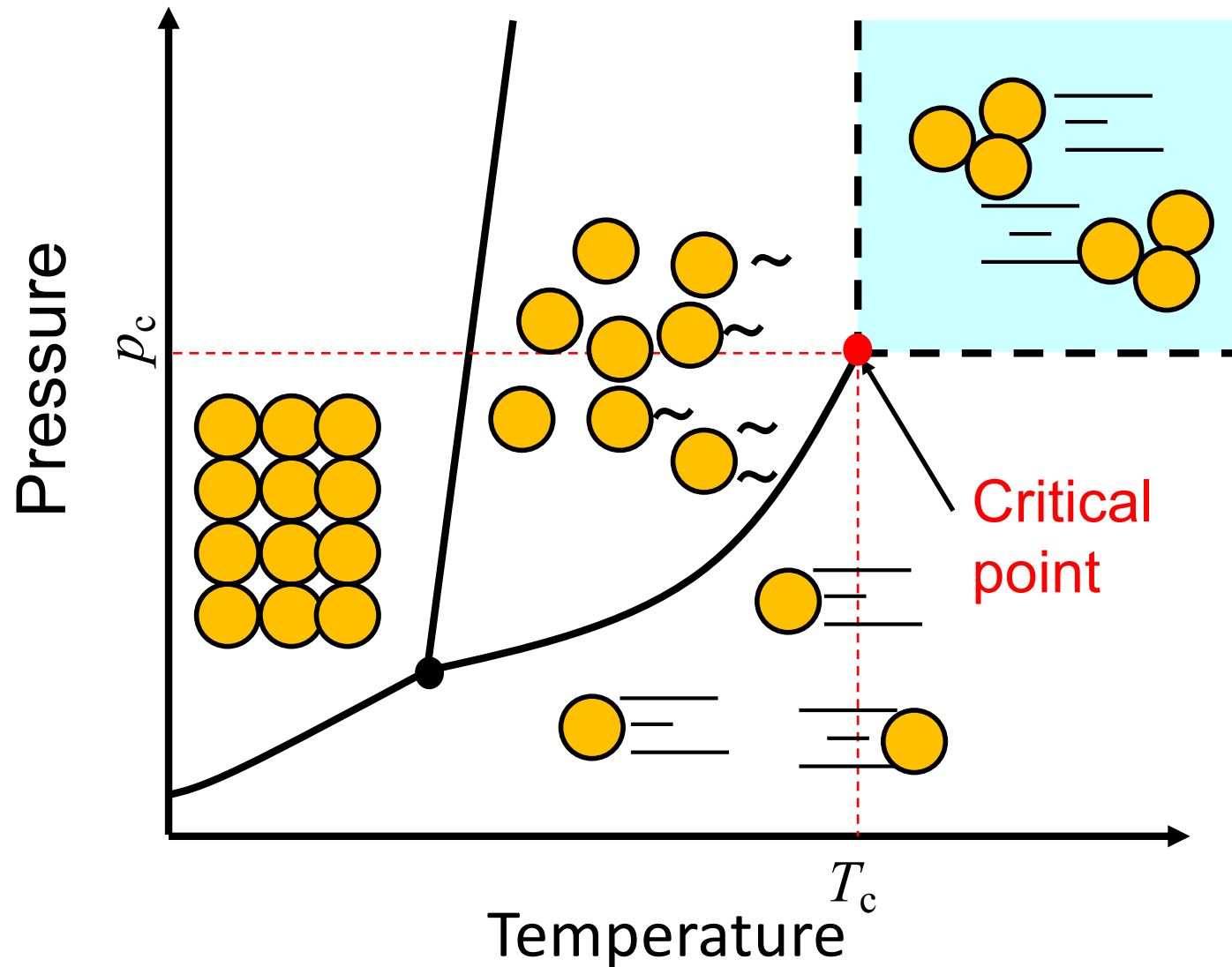
“超臨界流体入門”，化学工学会超臨界流体部会編，
丸善，2008



➤ Critical temperature and pressure

Substance	$T_c / ^\circ\text{C}$	p_c / MPa
H ₂	-240.0	1.30
H ₂ O	374.1	22.04
CO ₂	31.0	7.37
Toluene	318.5	4.11
Ethanol	239.4	8.09

- Molecular motion on solid, liquid, gas and SCF



➤ Application of SCF : Extraction

Raw Material		Extracted solute
Coffee beans, tea leaf		Caffeine (alkaloid)
Algae		β -carotene, carotenoid
Aroma	Vanilla beans	vanilline
	Citrus skin	Citrus oil
	Tea, green tea	Aqueous aromatic compound
Red pepper, paprika		capsicin
Fish oil		EPA and DHA

➤ Application of SCF : Extraction



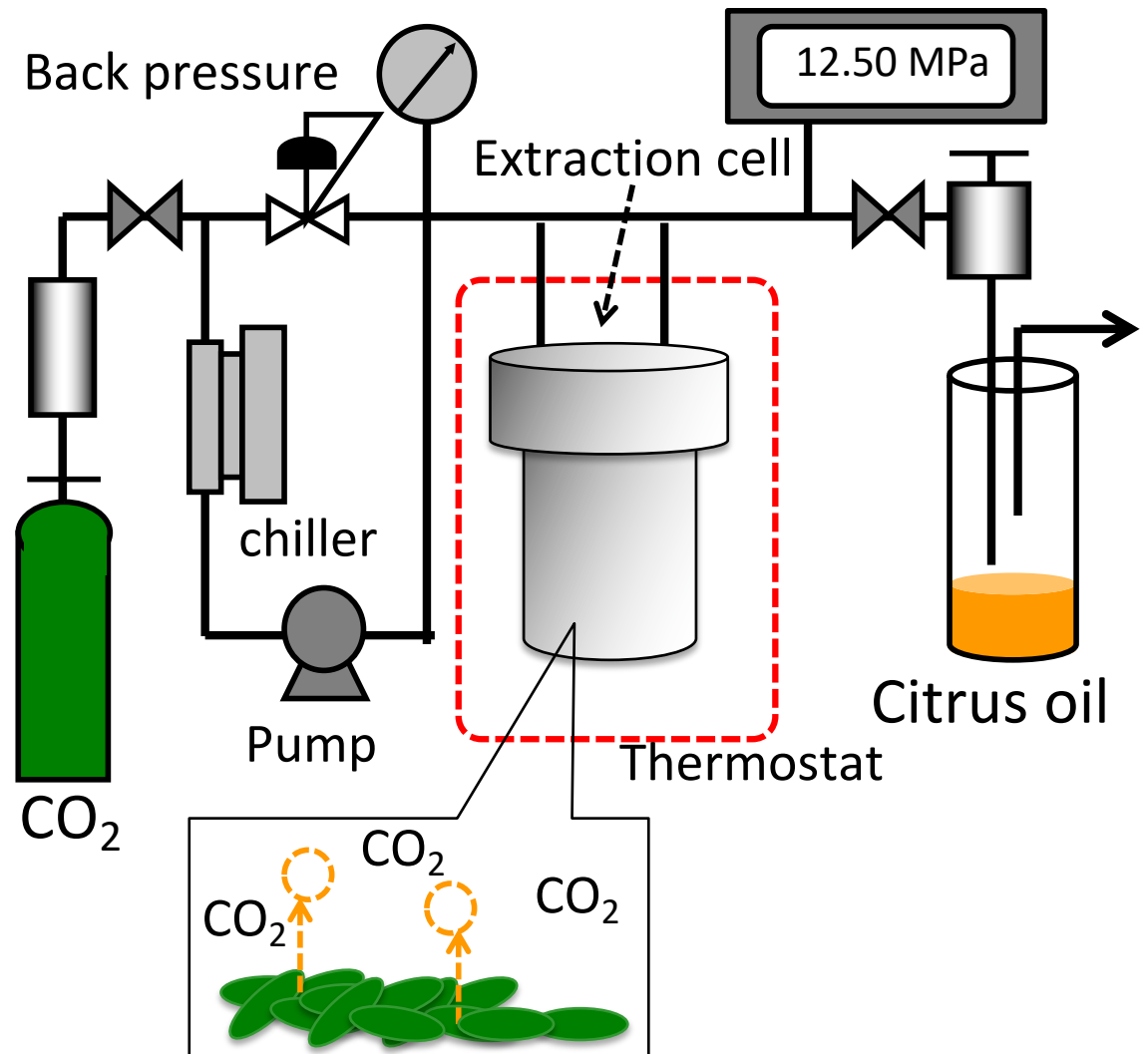
Raw material : Eucalyptus leaf

Condition: 50°C, 9 MPa

Extracted solute:

α -pinene (10.5 %)

1,8-cineole (62.6 %)



Flavor and Fragrance J., 14, 214 – 218 (1999).

Q 1-1. Application of SCF : Extraction

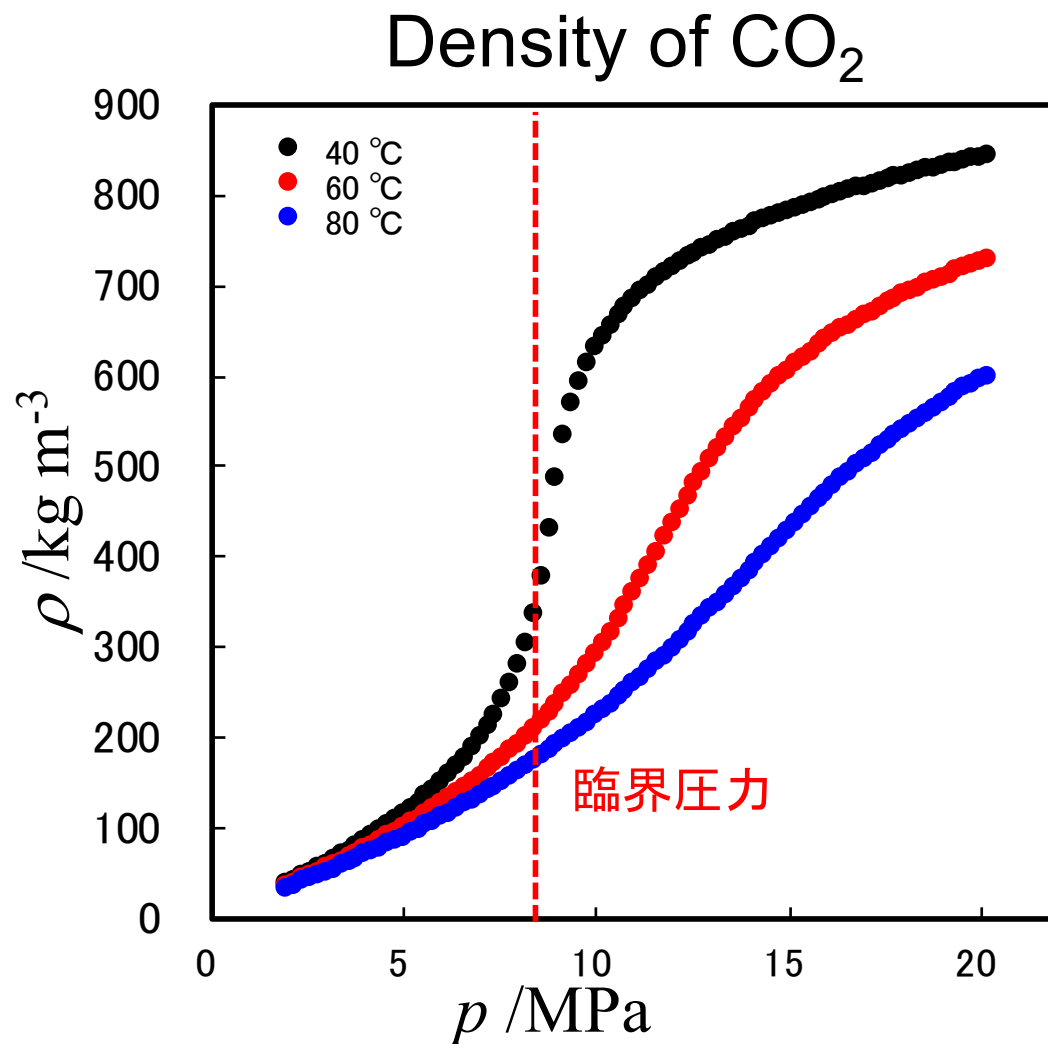
What is the advantage of extraction process using SCF compared to that using liquid solvent?

A 1-1. Application of SCF : Extraction

➤ Application of SCF : Reaction

Solvent	Reaction type
SCCO ₂	Hydrogenation of unsaturated fatty acid (Ru, Rh catalyst)
	Hydroformylation (Rh, Co catalyst)
CO ₂ expand liquid	Oxidation and Hydrogenation: Enhanced dissolution of O ₂ , H ₂ to liquid phase
High temp. and press. water	Oxidation: Decomposition of toxic compounds
	Hydrogenation of heavy oil (NiMo, CoMo catalyst)
	Gasification of biomass (NaOH, KOH, Ni catalyst)
SCMeOH	Production of biodiesel from fat and oil

➤ Application of SCF : Material process



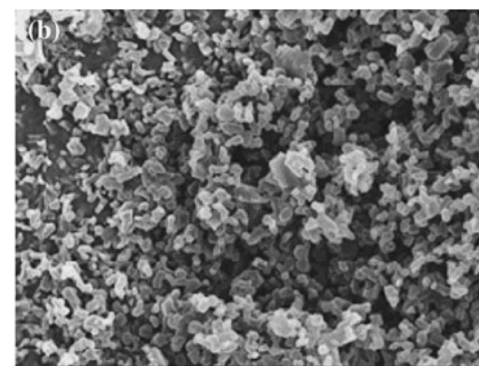
Diffusion coefficient, Viscosity

Solubility in supercritical CO₂

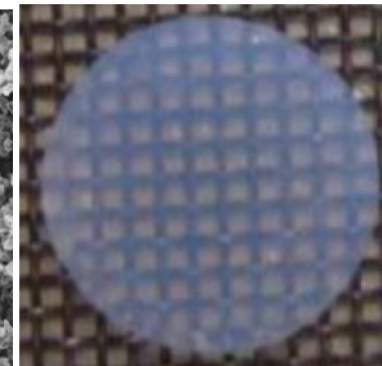
Phase equilibria and phase behavior



Design of Material Process



nanoparticle



Aerogel

Bozbag, S. E. et al., J. Mater. Sci., 47 (2012) 2995 – 3025.

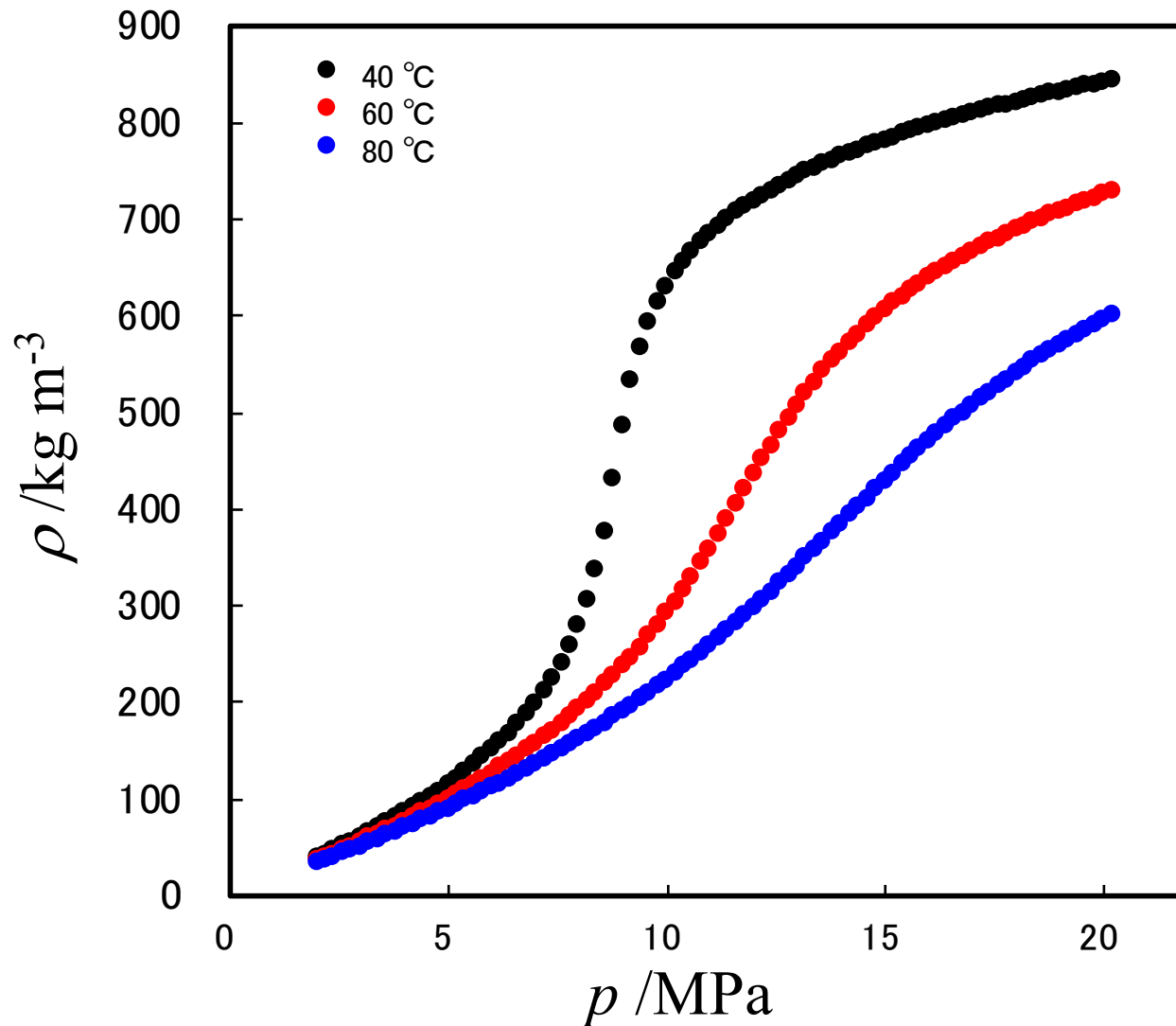
Sanli, D. et al., J. Mater. Sci., 47 (2012) 3469 – 3492.

➤ Property of gas, liquid and supercritical fluid

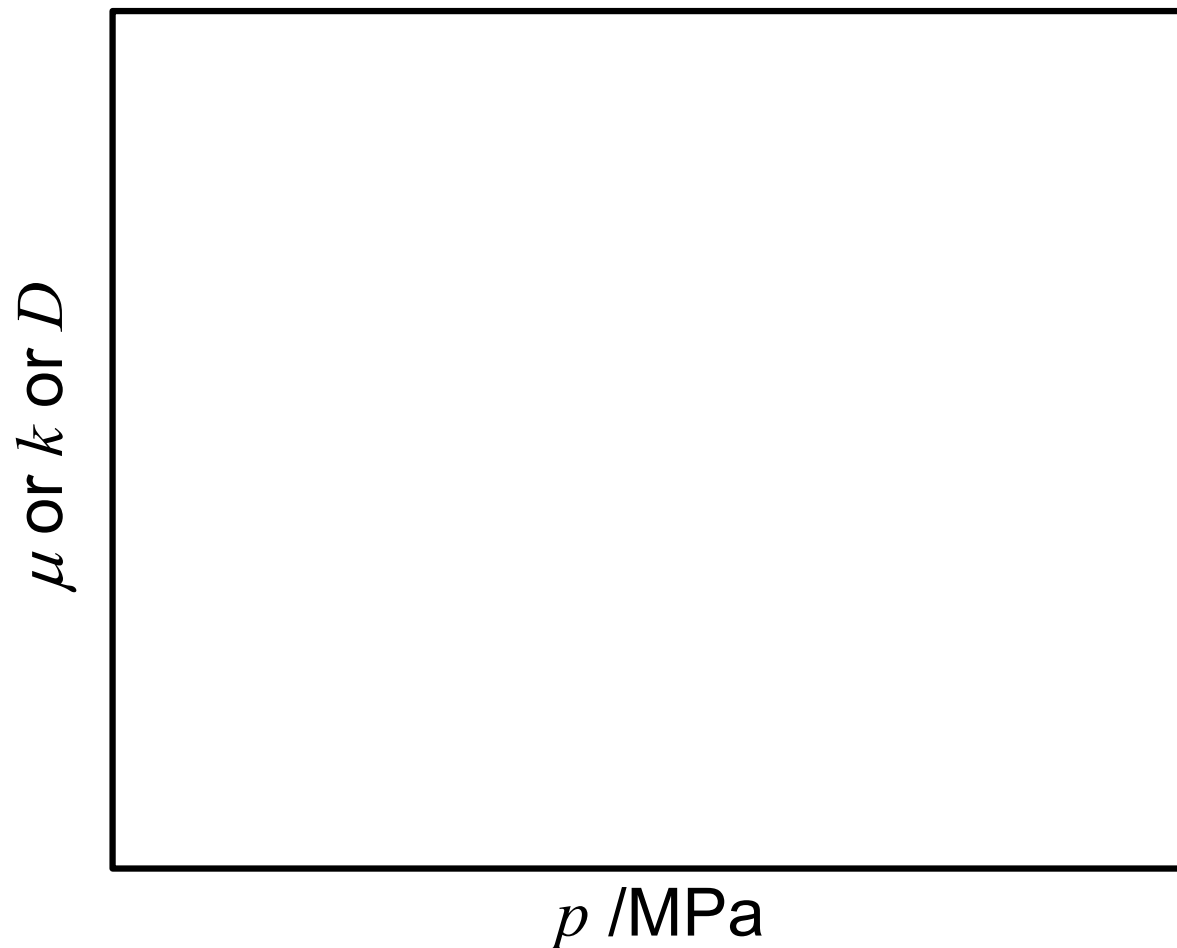
	Gas	Supercritical Fluid	Liquid
density / kg m^{-3}	0.6 – 2	300 – 900	700 – 1600
diffusion coefficient/ $10^{-9} \text{ m}^2 \text{ s}^{-1}$	1000 – 4000	20 – 700	0.2 – 2
Viscosity / 10^{-5} Pa s	1 – 3	1 – 9	200 – 300
Thermal conductivity / $10^{-3} \text{ W m}^{-1} \text{ K}^{-1}$	1	1 – 100	100

➤ Density of CO₂

R. Span and W. Wagner,
J. Phys. Chem. Ref. Data 25(6), 1509–1596 (1996).



Q.1-2: What is the behavior of viscosity μ , thermal conductivity k and diffusion coefficient D as the function of pressure at constant temperature?

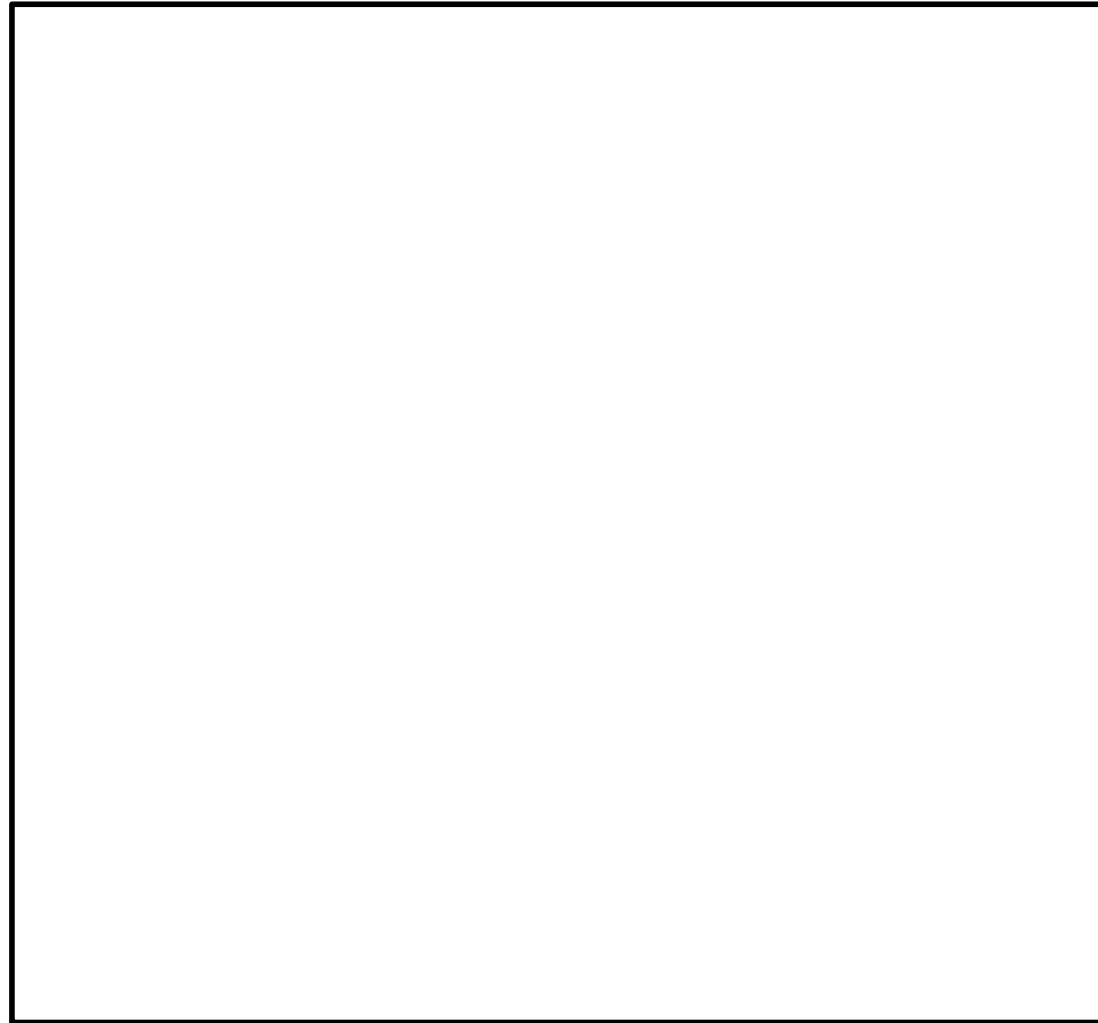


A. 1-2

R. Span and W. Wagner,
J. Phys. Chem. Ref. Data 25(6), 1509–1596 (1996).

Viscosity

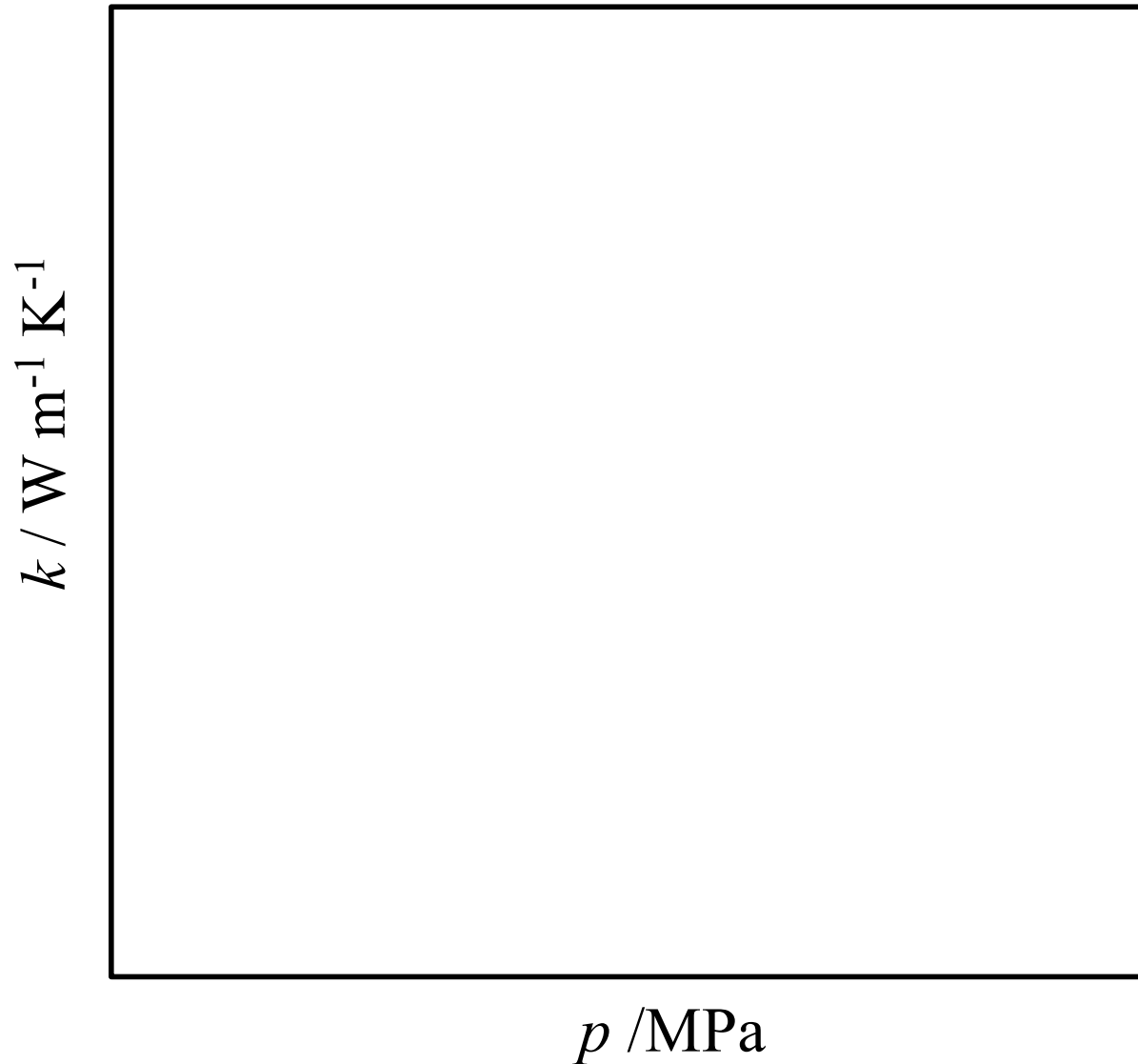
$\mu \times 10^5 / \text{Pa s}$



p / MPa

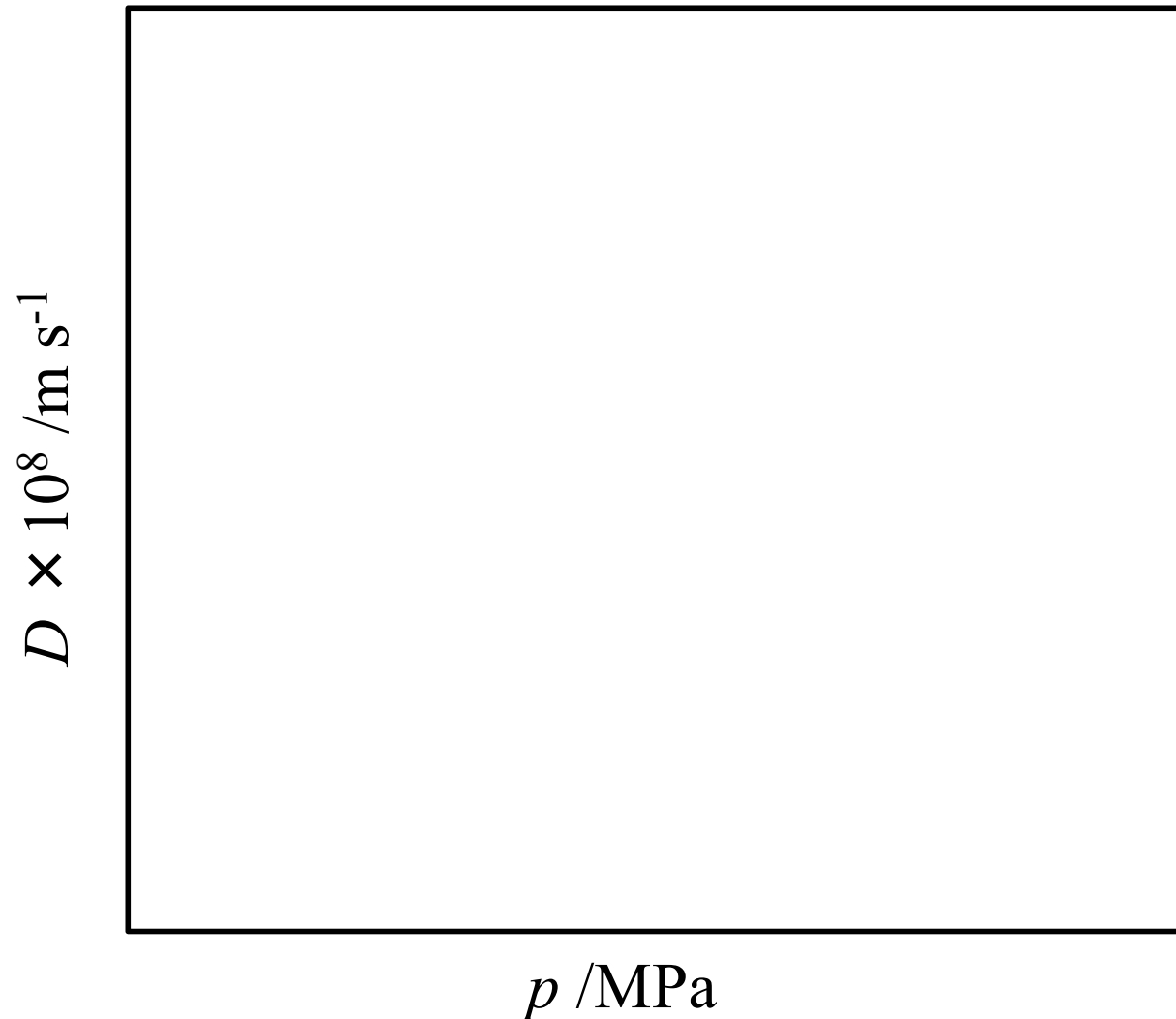
A. 1-2

Thermal conductivity



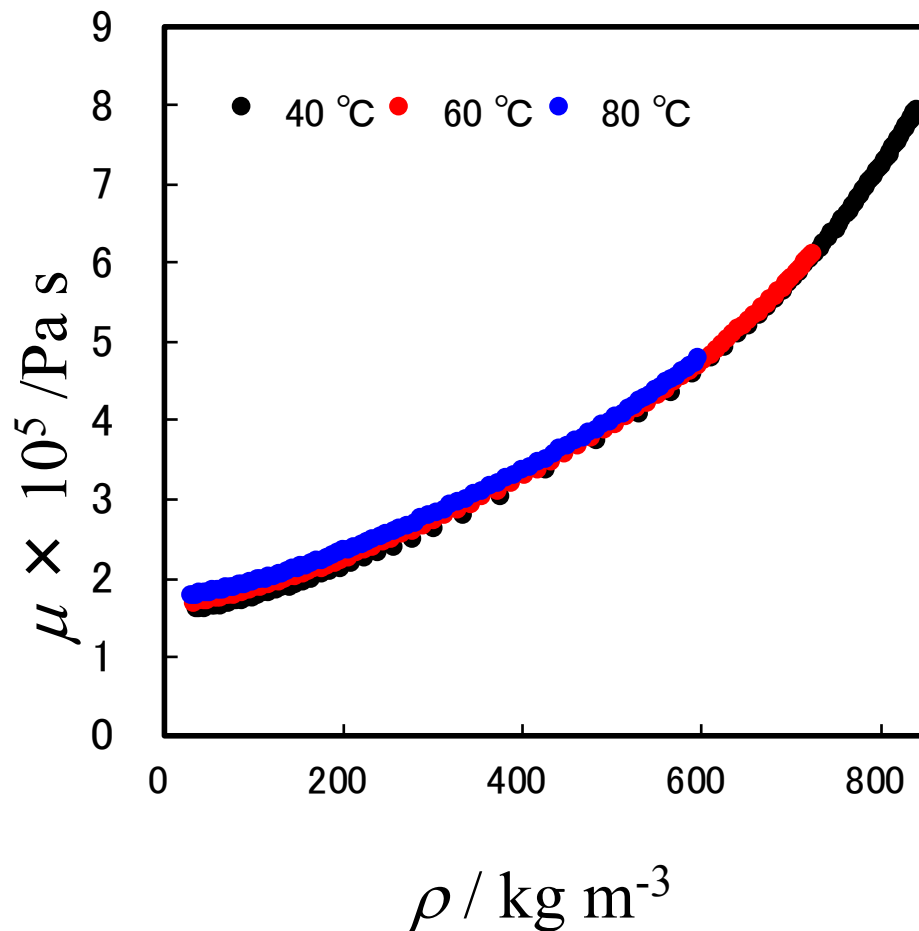
A. 1-2

Diffusion coefficient of naphthalene

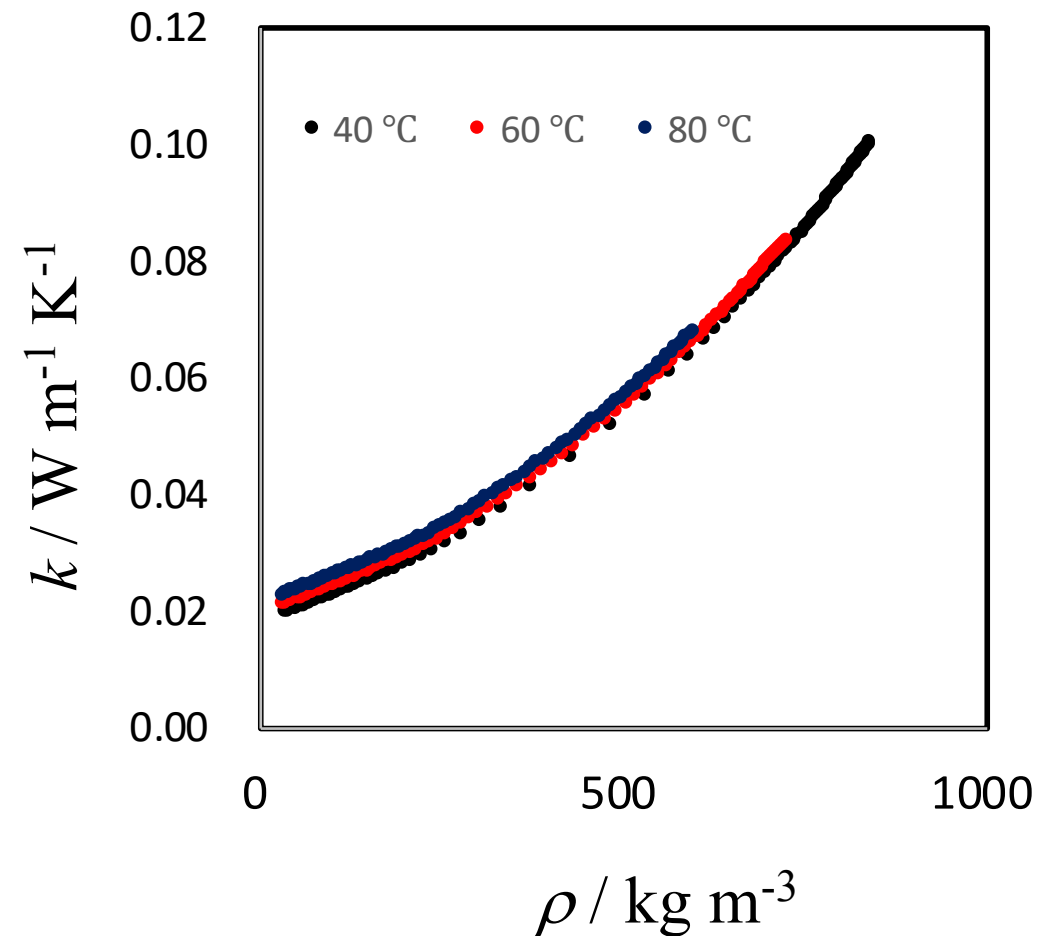


- If the function of density,

Viscosity

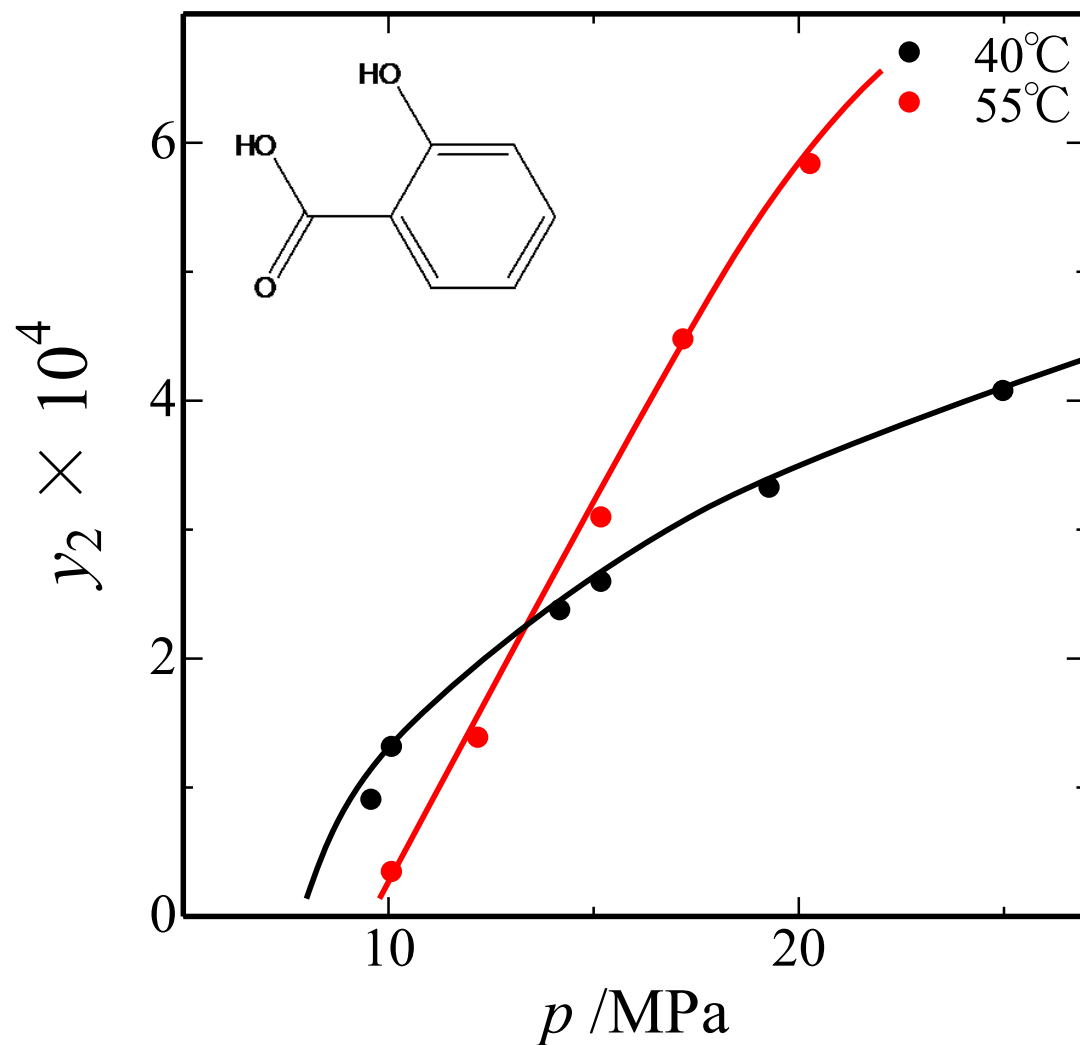


Thermal conductivity



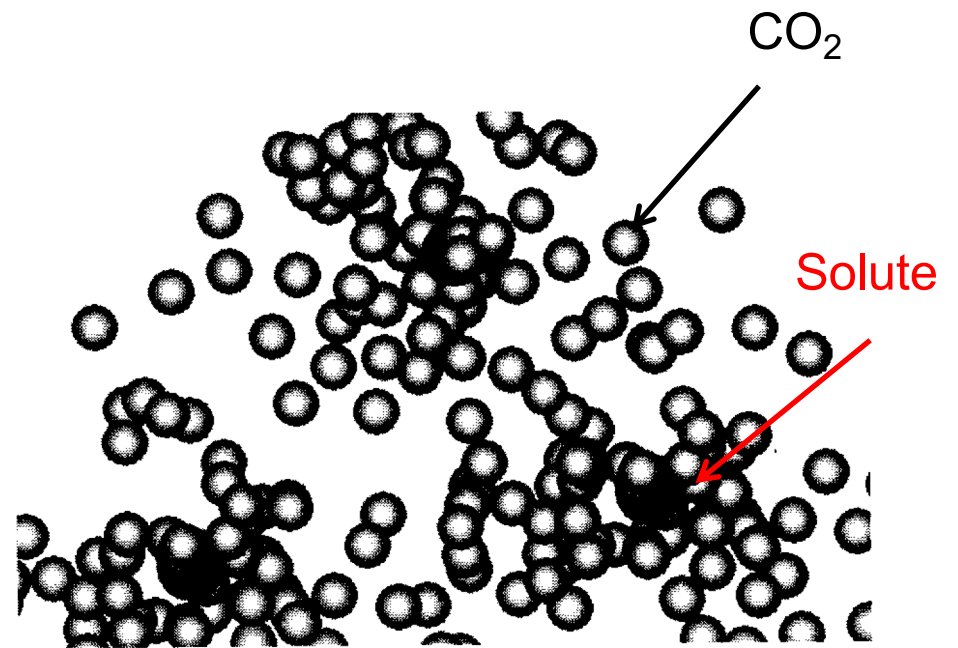
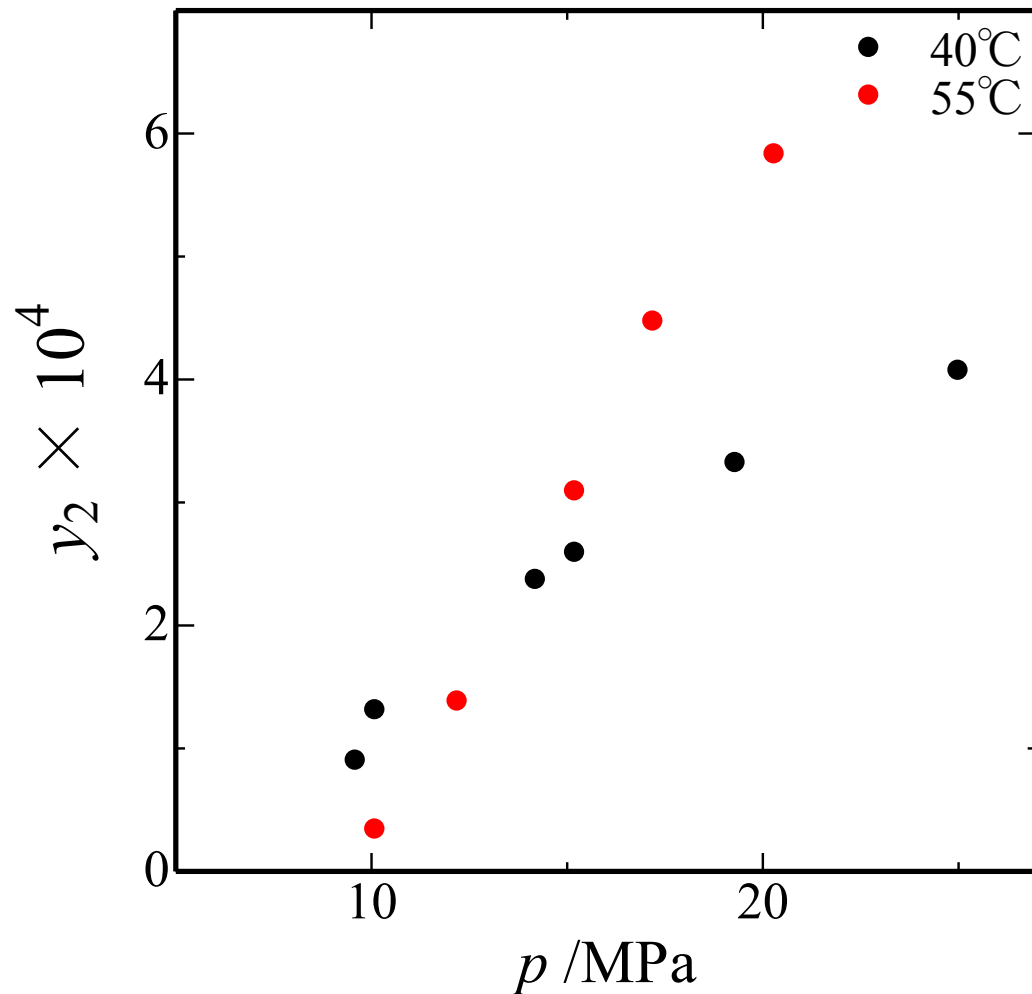
Solubility of salicylic acid in supercritical CO₂

Haung, Z., J. Chem. Eng. Data, 49 (2009) 1323 – 1327.



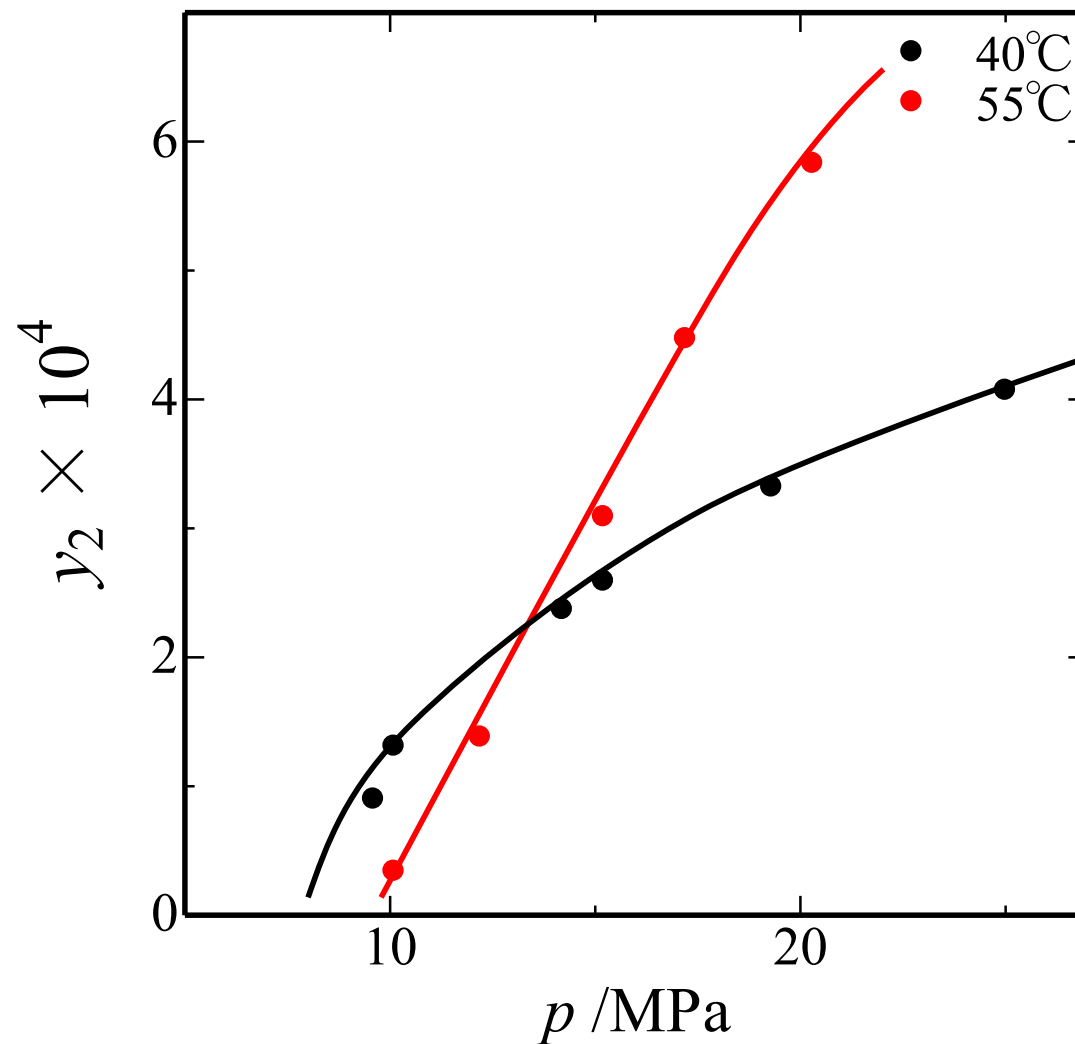
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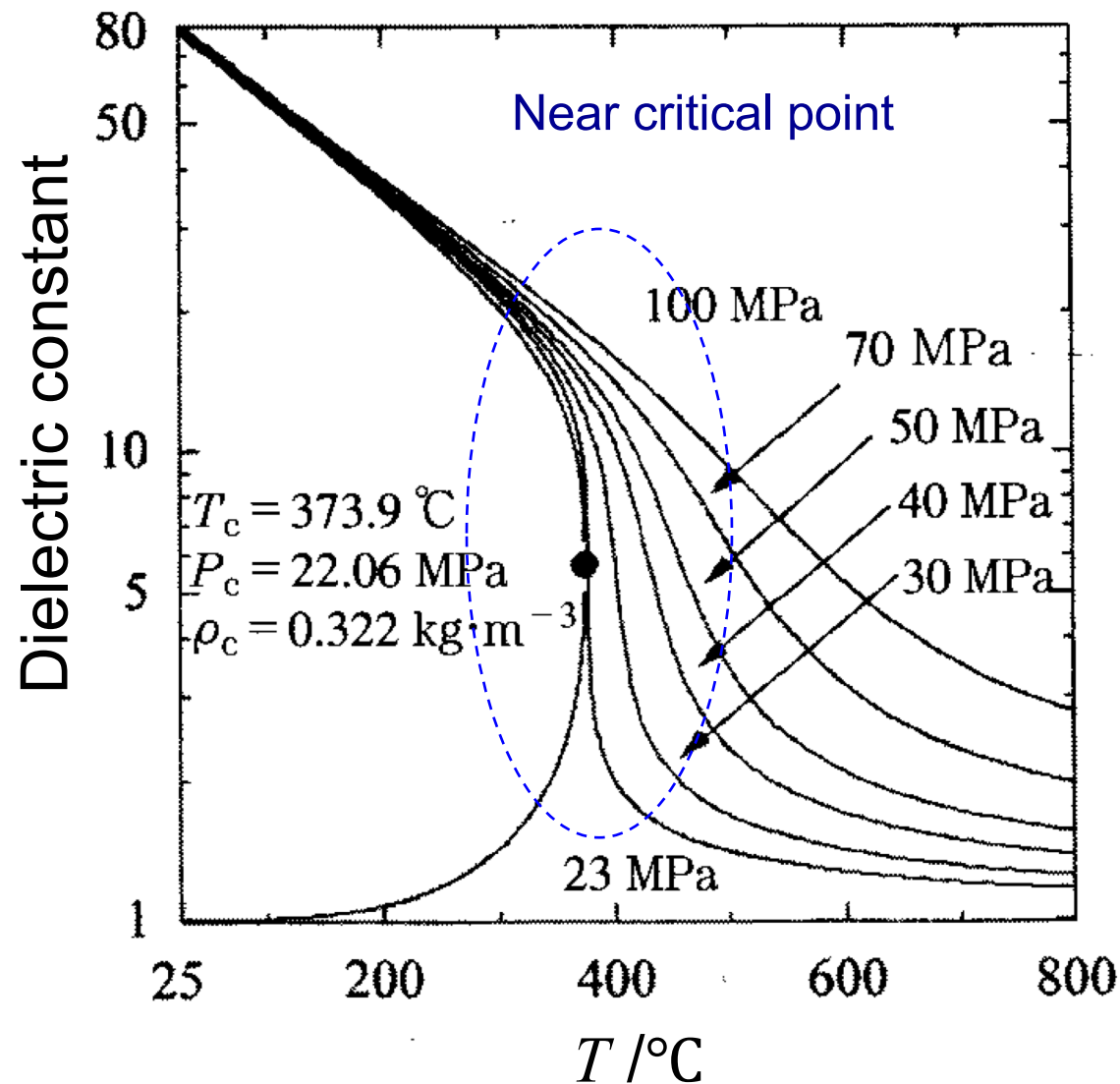
Cluster structure from molecular simulation

Q. 1-3: Why is the cross over point of solubility in supercritical carbon formed?

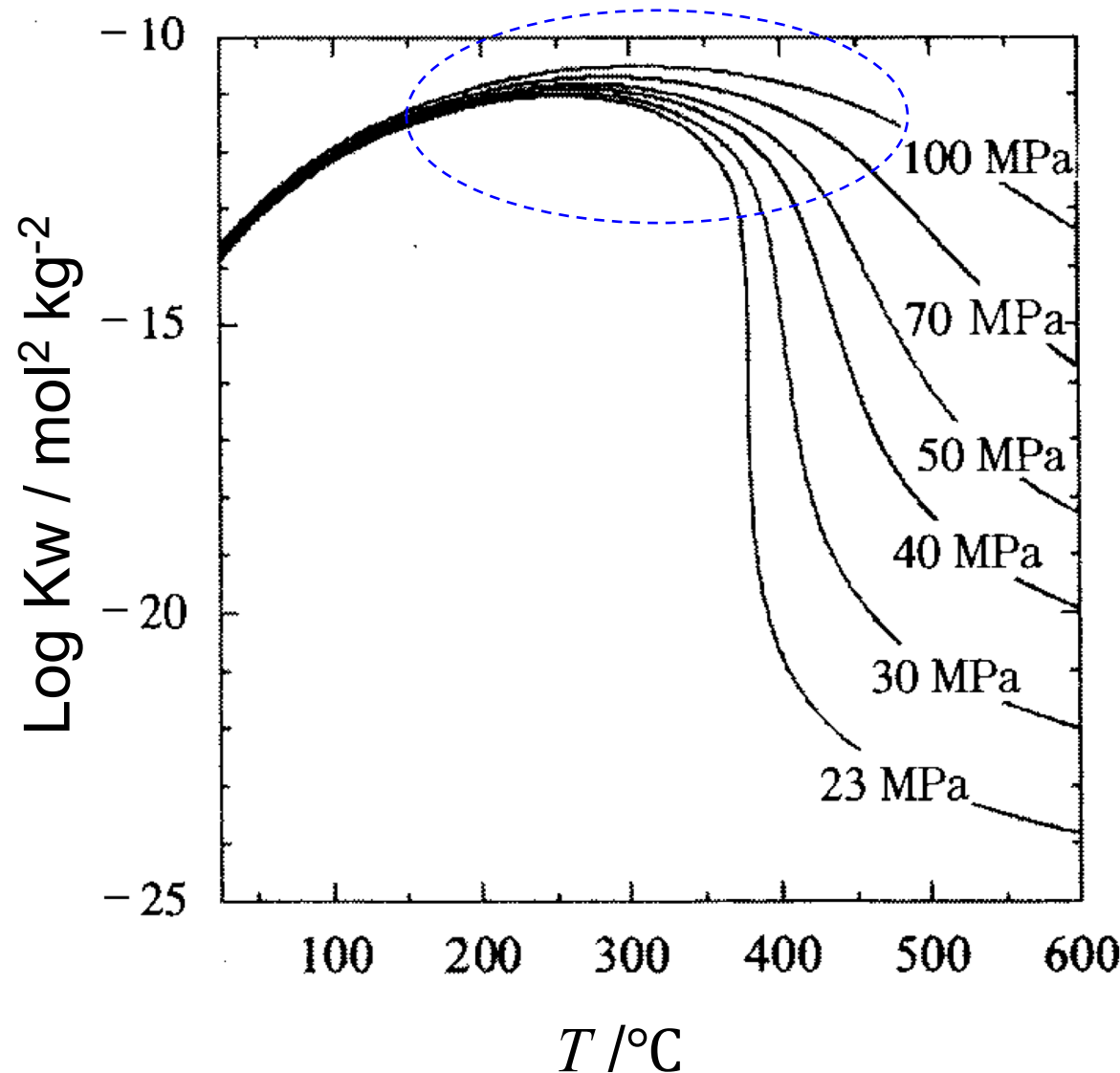


A. 1-3:

- Supercritical water (high temperature and pressure water)



- Supercritical water (high temperature and pressure water)



Dissociation of water



K_w : Ionic product

- Maximum at 300 °C
- Enhancement of hydrolysis

➤ Supercritical water (high temperature and pressure water)

➤ Ultraheavy oil*

- ✓ Canada: Oilsand
333 Billion Barrel
- ✓ Venezuela: Orinoco Tar
289 Billion Barrel
- ✓ Current Oil: 1000 Billion Barrel



Oilsand
(Canada)

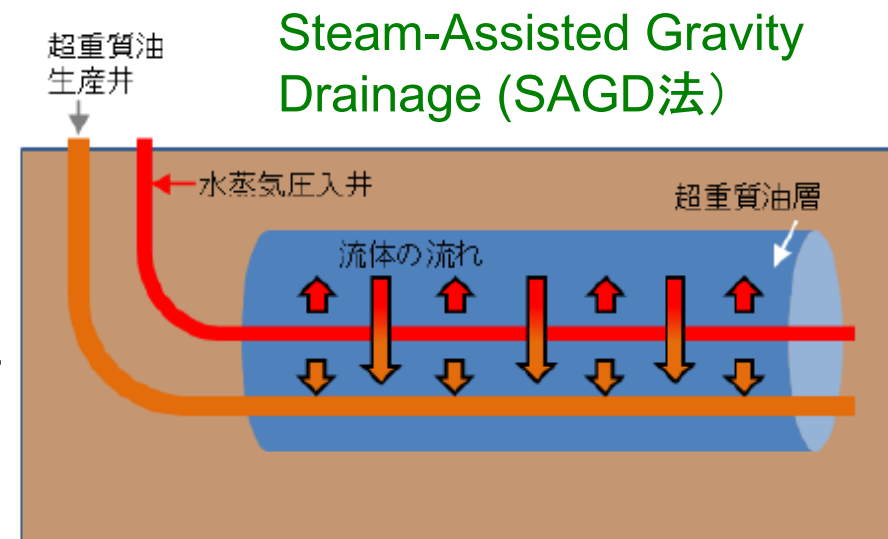


Orinoco Tar
(Venezuela)

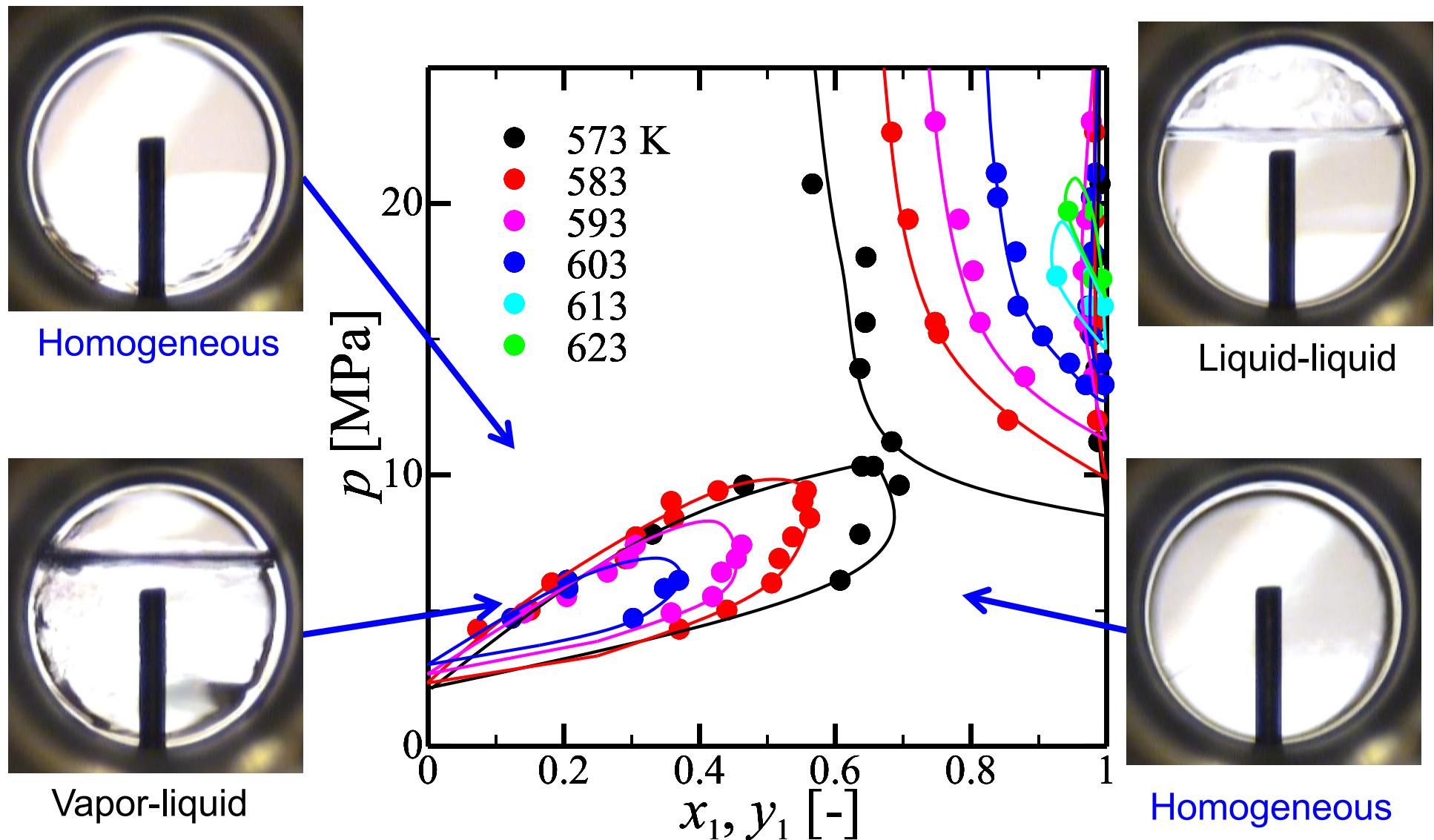
➤ Upgrading of Ultraheavy oil*

SAGD : Using high-temperature and pressure water

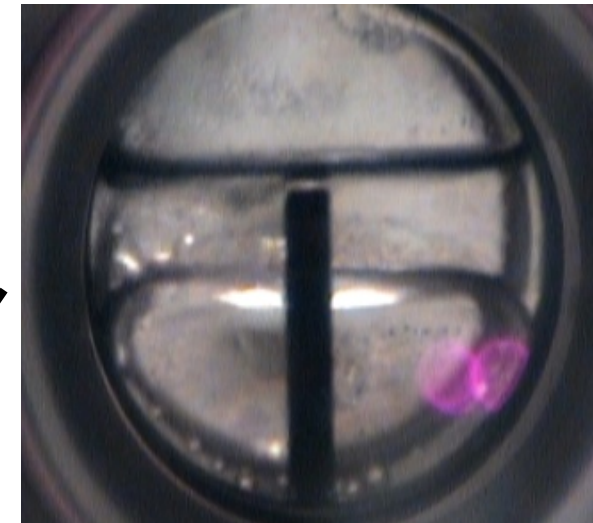
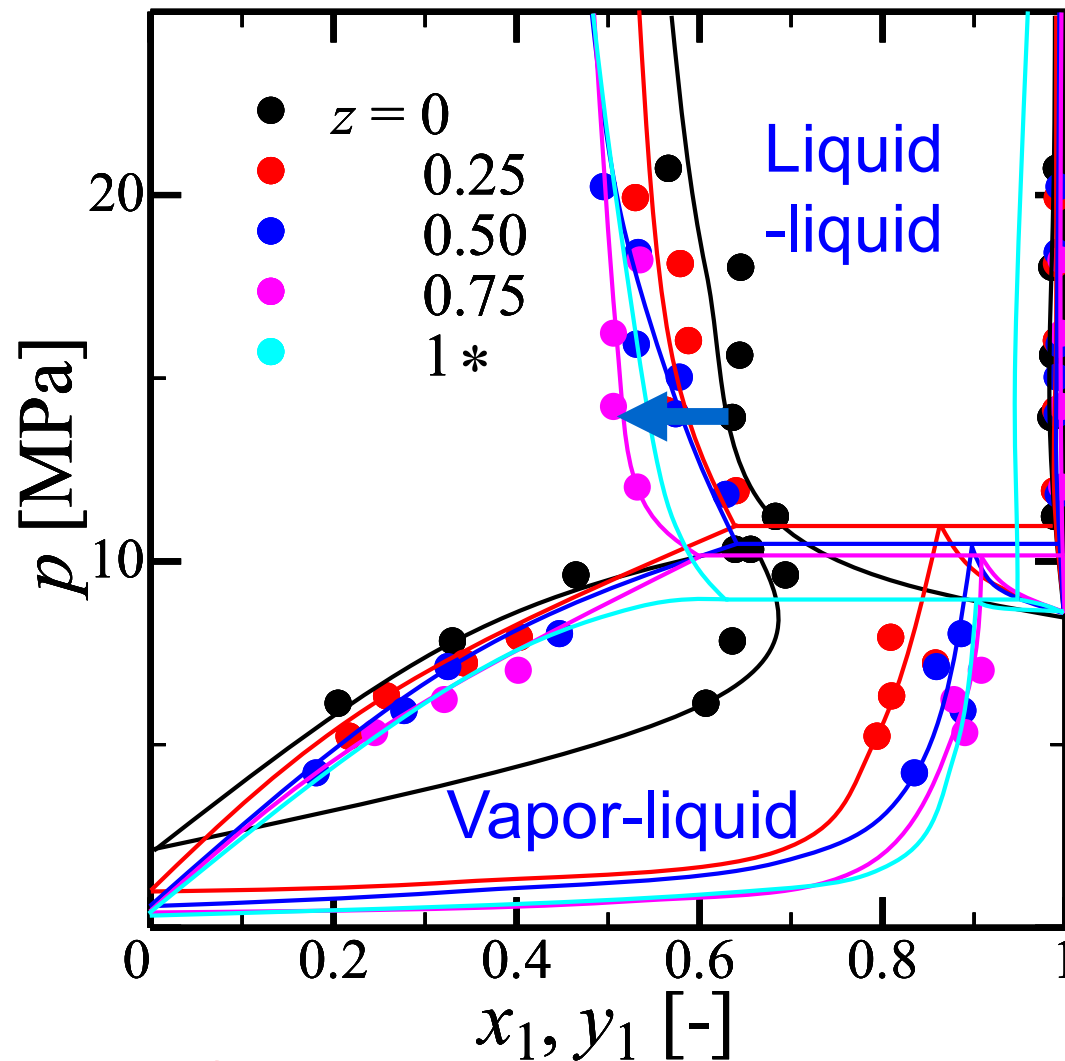
Upgrading : reduction of viscosity, light oil production, desulfurization



➤ Supercritical water (high temperature and pressure water)



- Supercritical water (high temperature and pressure water)

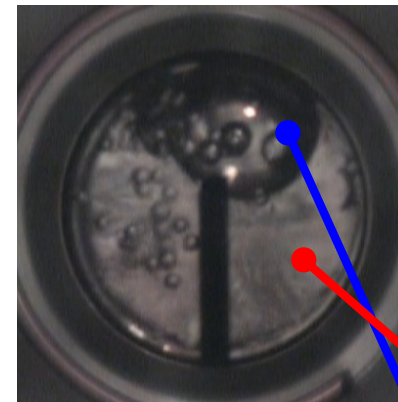
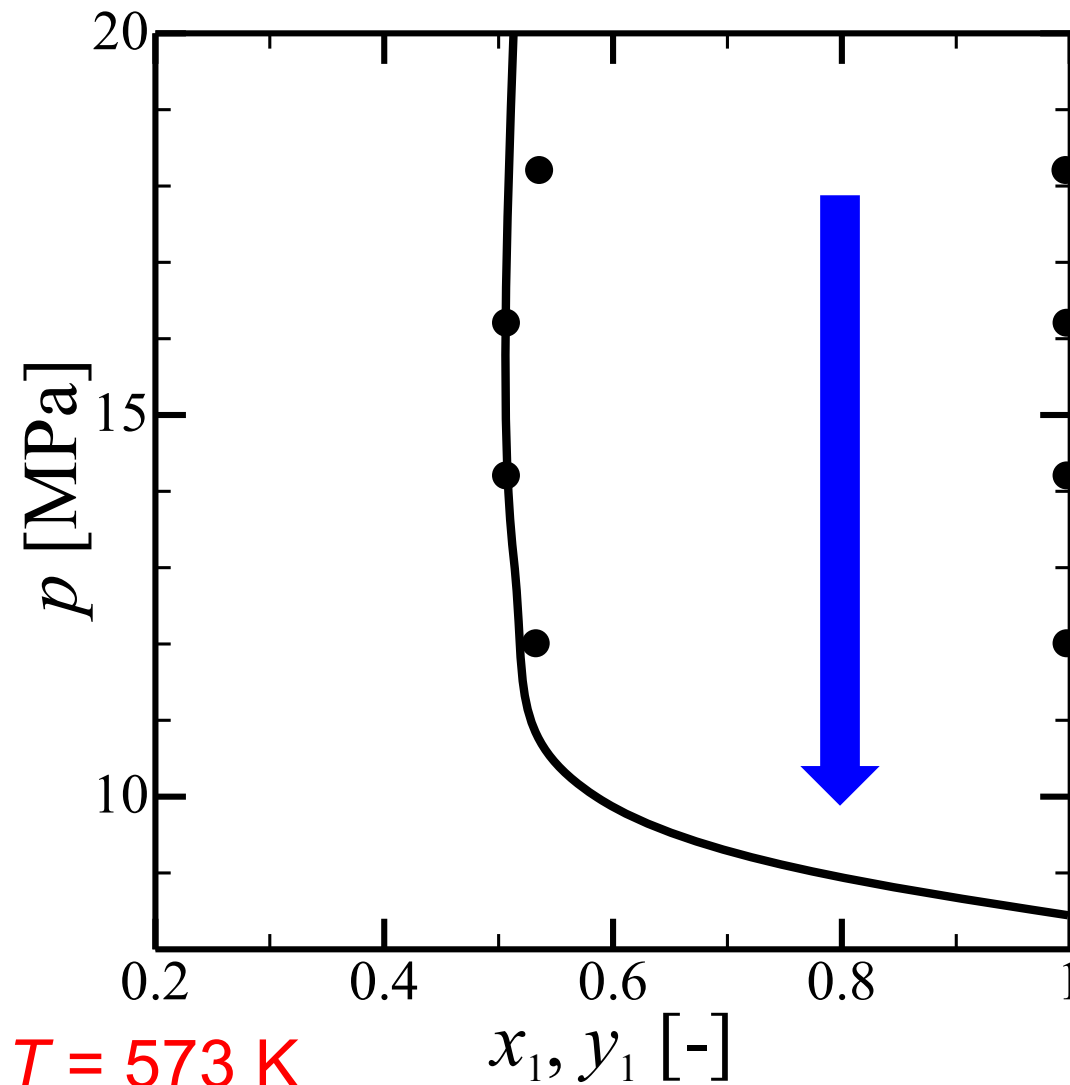


Vapor-liquid-liquid (VLE)

$T = 573$ K

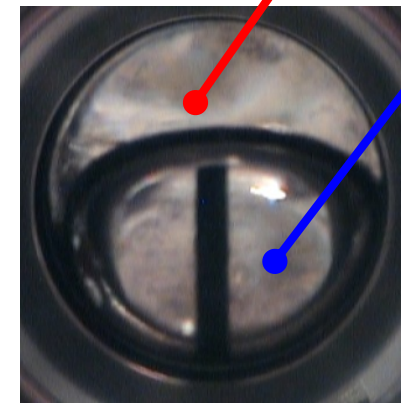
➤ Supercritical water (high temperature and pressure water)

Phase transition on liquid-liquid equilibria



22 MPa

Hydrocarbon rich



12 MPa

Water rich

➤ Supercritical water (high temperature and pressure water)

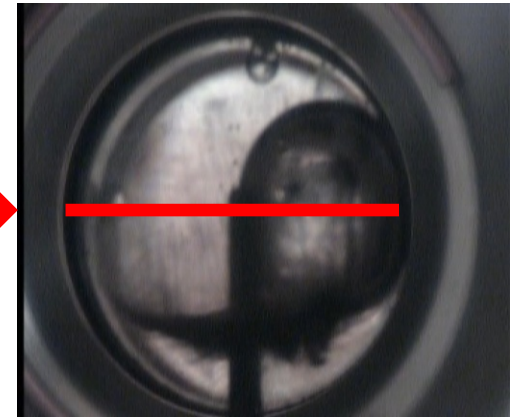
Mole ratio heavy oil / light oil = 0.75



25.0MPa



24.5MPa



24.4MPa

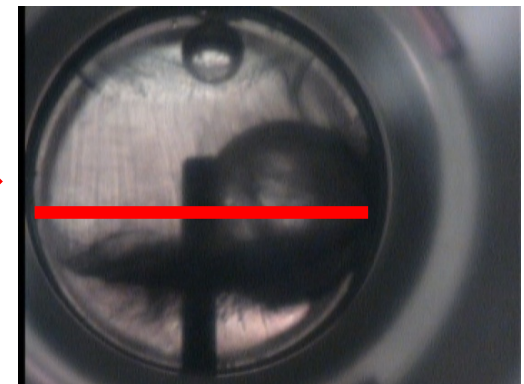
Mole ratio heavy oil / light oil = 0.80



20.5MPa

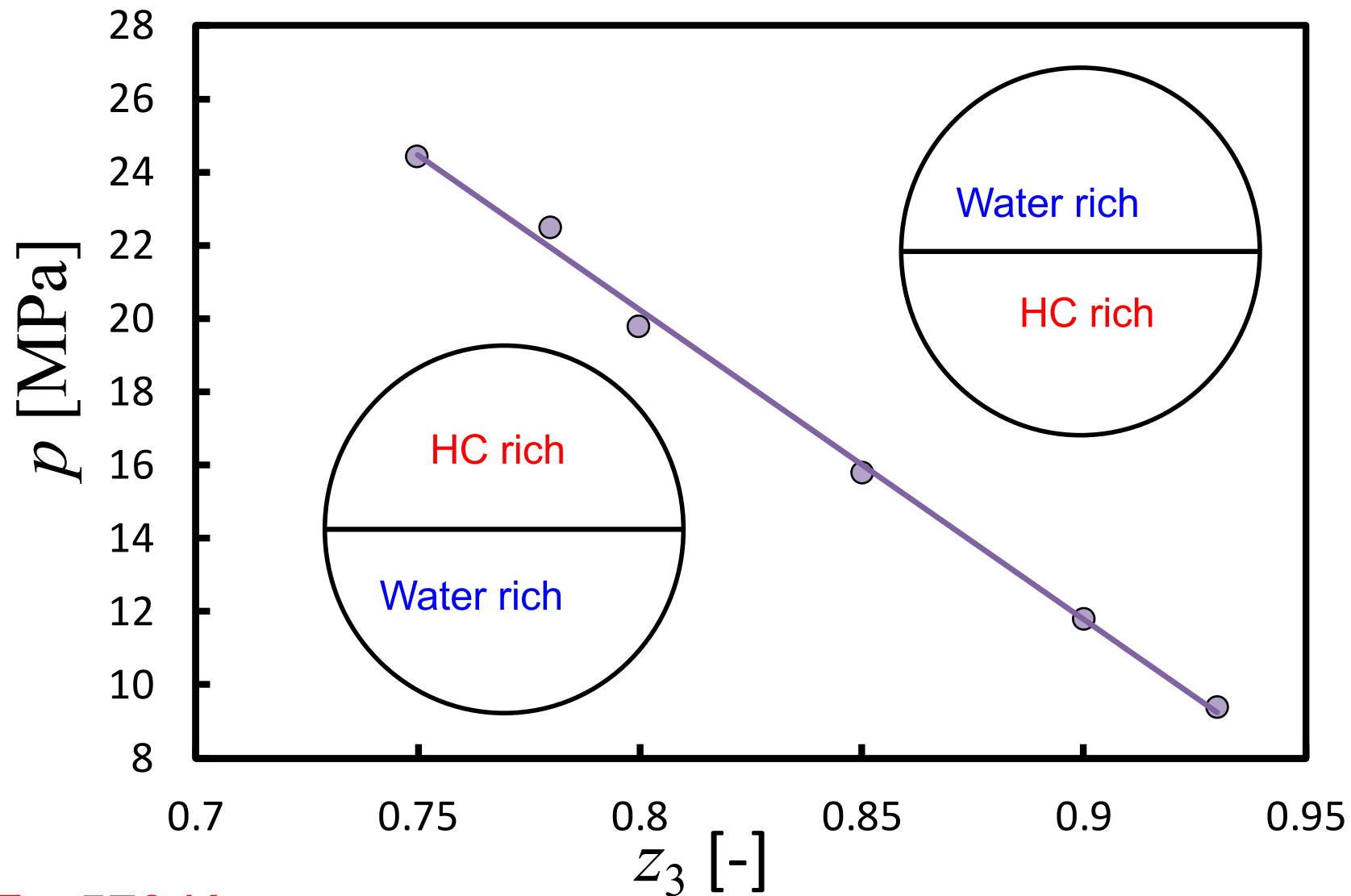


20.1MPa



19.9MPa

- Supercritical water (high temperature and pressure water)



$T = 573 \text{ K}$

Q. 1-4: Why is this phase transition on liquid-liquid two phase region formed?



High pressure

Low pressure